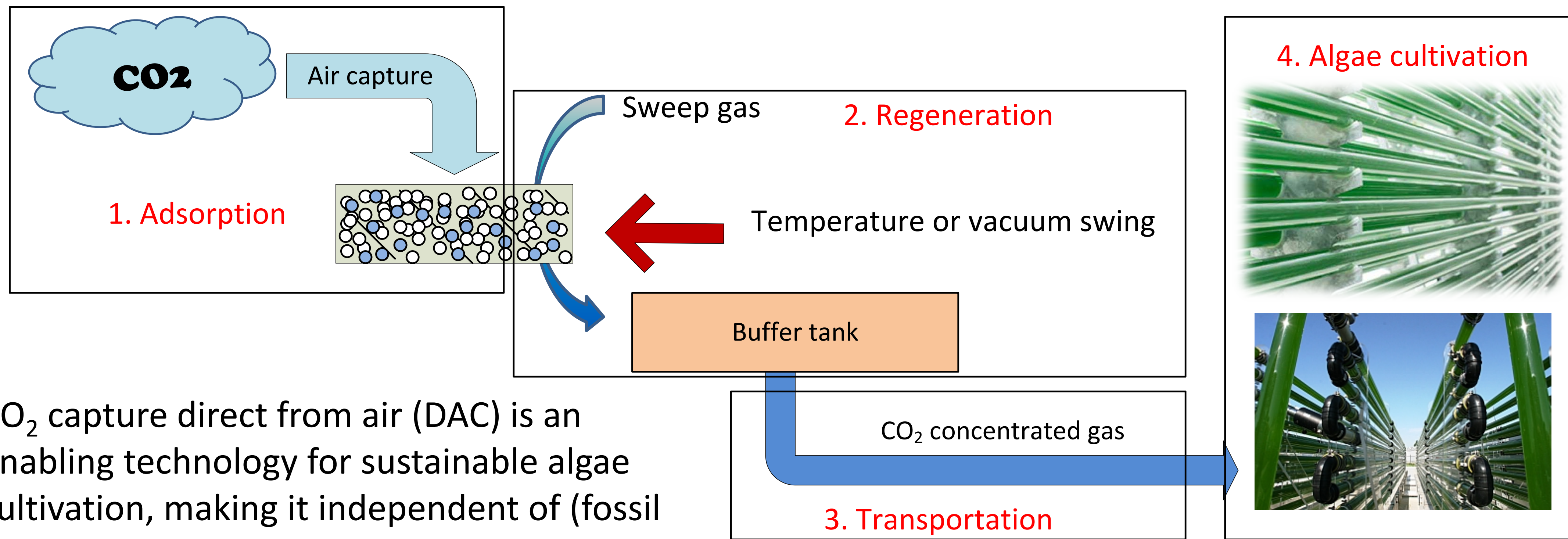


# CO<sub>2</sub> concentration from air for microalgae cultivation

## Introduction



CO<sub>2</sub> capture direct from air (DAC) is an enabling technology for sustainable algae cultivation, making it independent of (fossil based) CO<sub>2</sub> sources as flue gases.

### Sorbent-based CO<sub>2</sub> capture:

- ✓ no solvent evaporation
- ✓ low specific heat
- ✓ fast sorption kinetics
- ✓ higher CO<sub>2</sub> capacity?
- ✓ Stability?

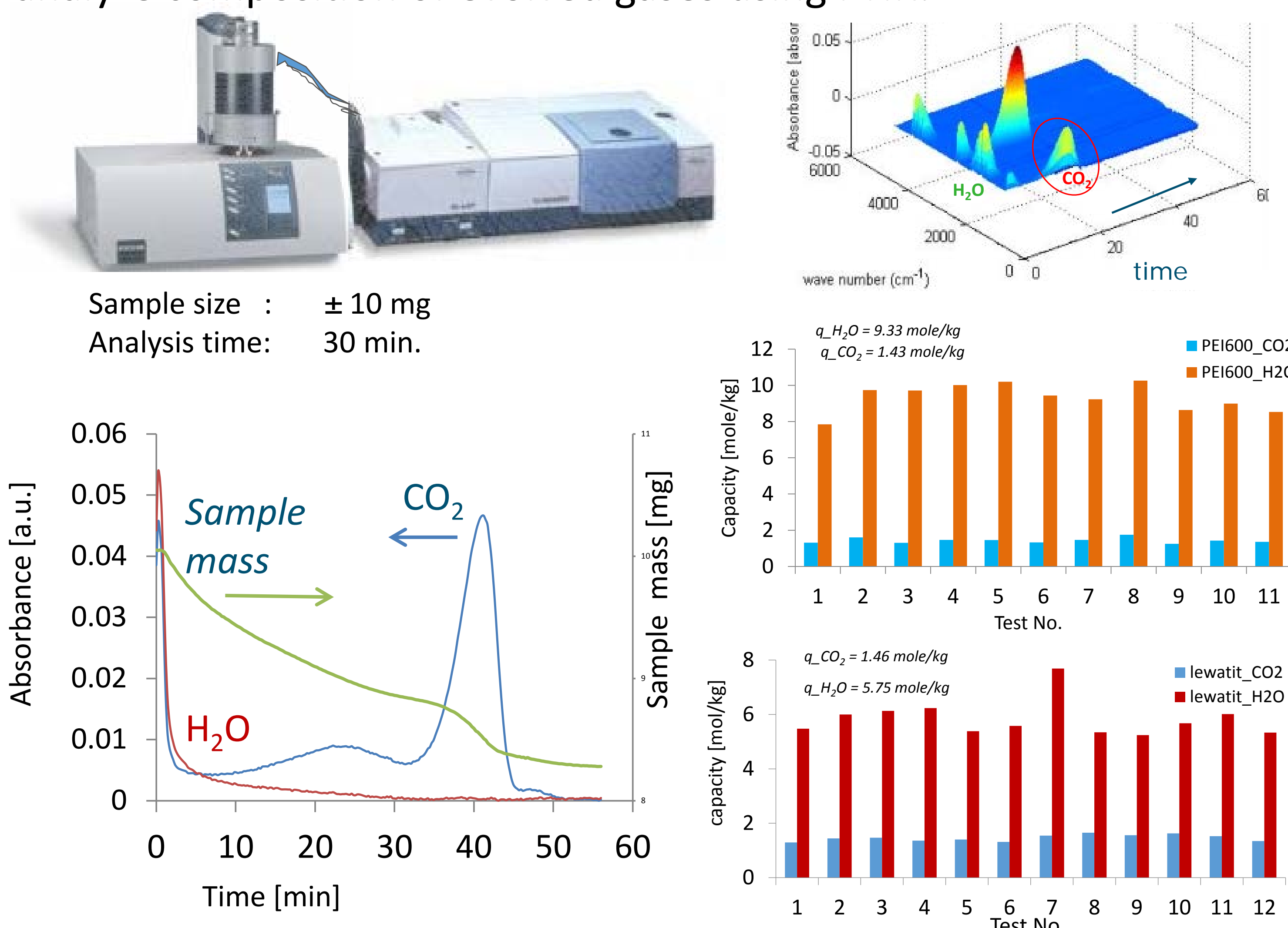
### Production of ...

- (1) CO<sub>2</sub> enriched air (open PBRs)
- (2) Pure CO<sub>2</sub> (closed PBRs)

## Sorbent Selection

- Ideal sorbents for DAC: 1) High CO<sub>2</sub> capacity  
2) High selectivity of CO<sub>2</sub> over H<sub>2</sub>O

Principle: measure sample mass loss during heating in TGA and analyze composition of evolved gases using FTIR.



Sample size : ± 10 mg  
Analysis time: 30 min.

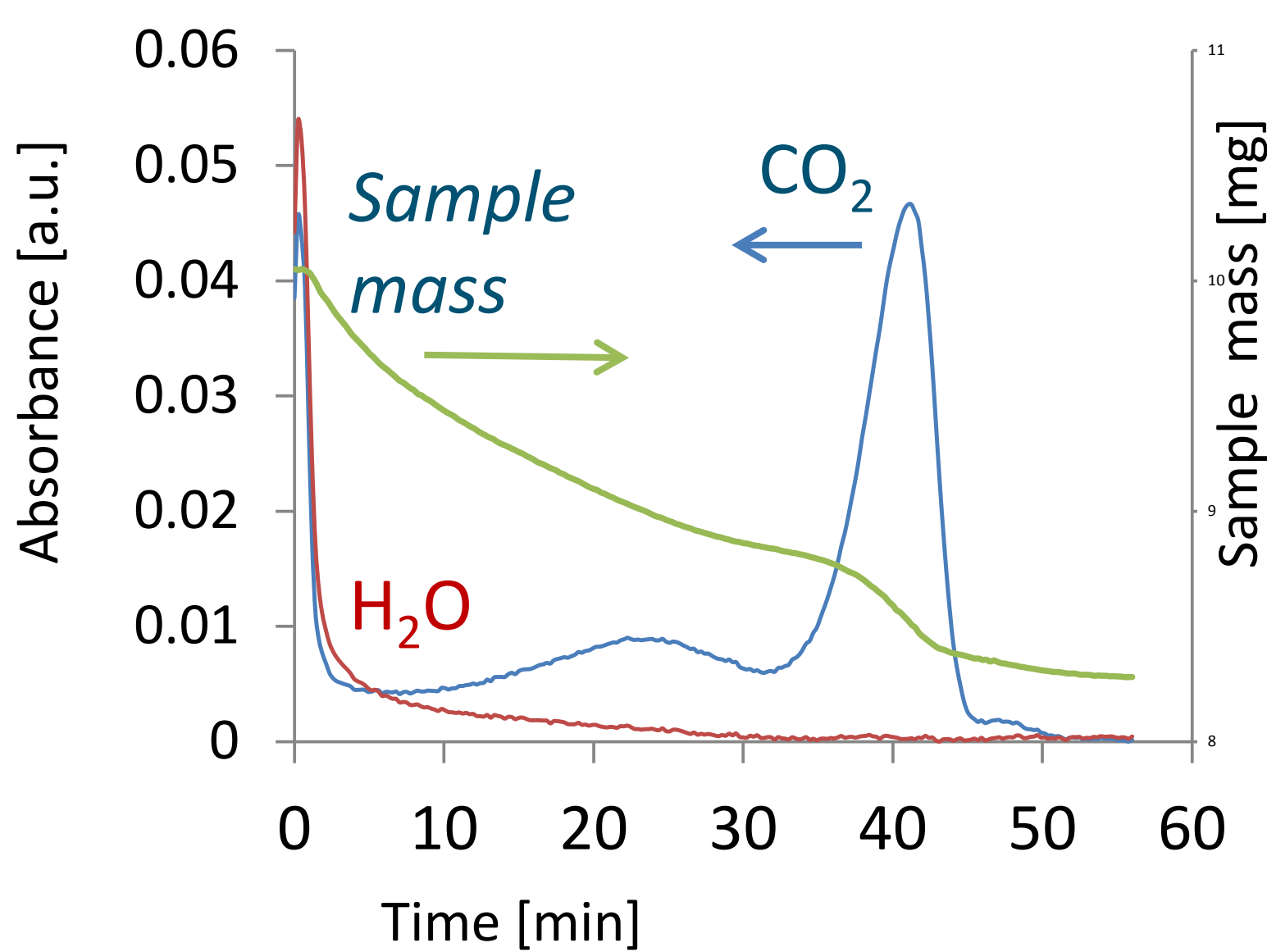


Figure 1: screening sorbents for direct air capture at ambient (lab) conditions for 15h

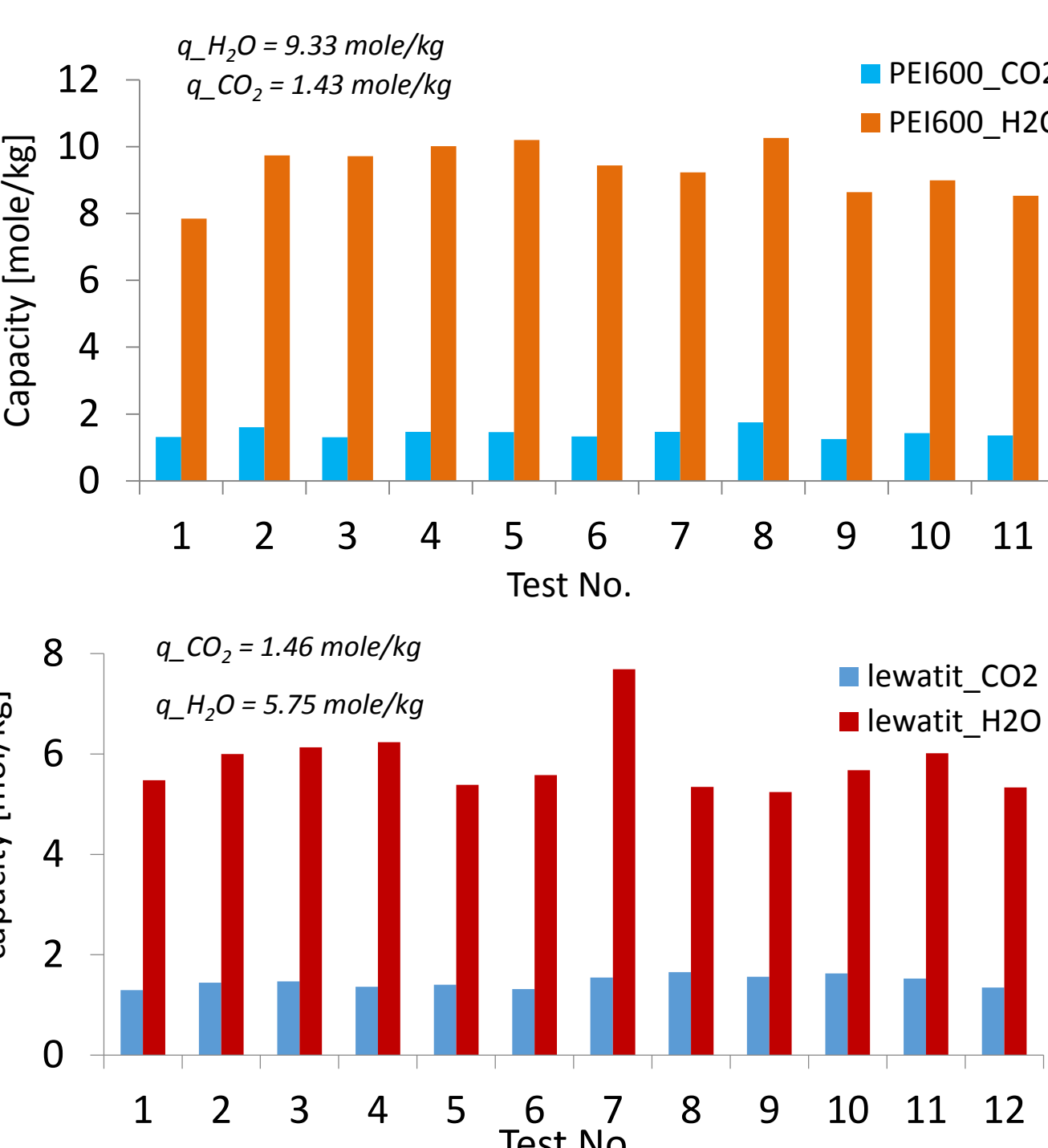


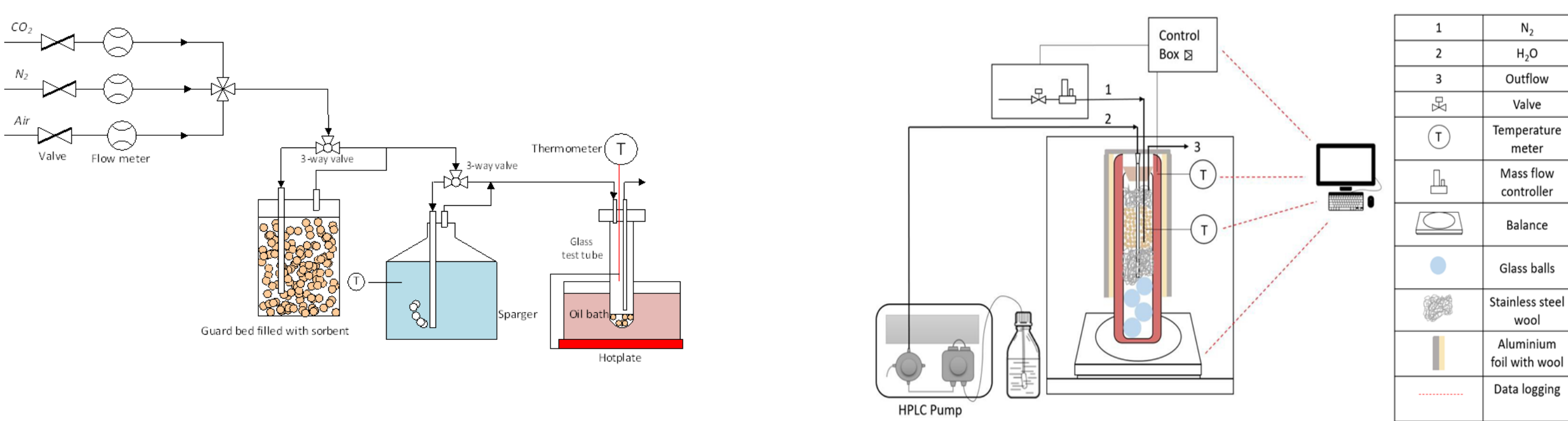
Figure 2: reproducibility tests of PEI600 (above) and Lewatit IER (below)

## Sorbent Characterization (1): Stability

To evaluate sorbent stability under diff. (desorption) conditions

Continuous treatment:

Cyclic operation:



Stability in air, CO<sub>2</sub>, N<sub>2</sub> and H<sub>2</sub>O at elevated temperature

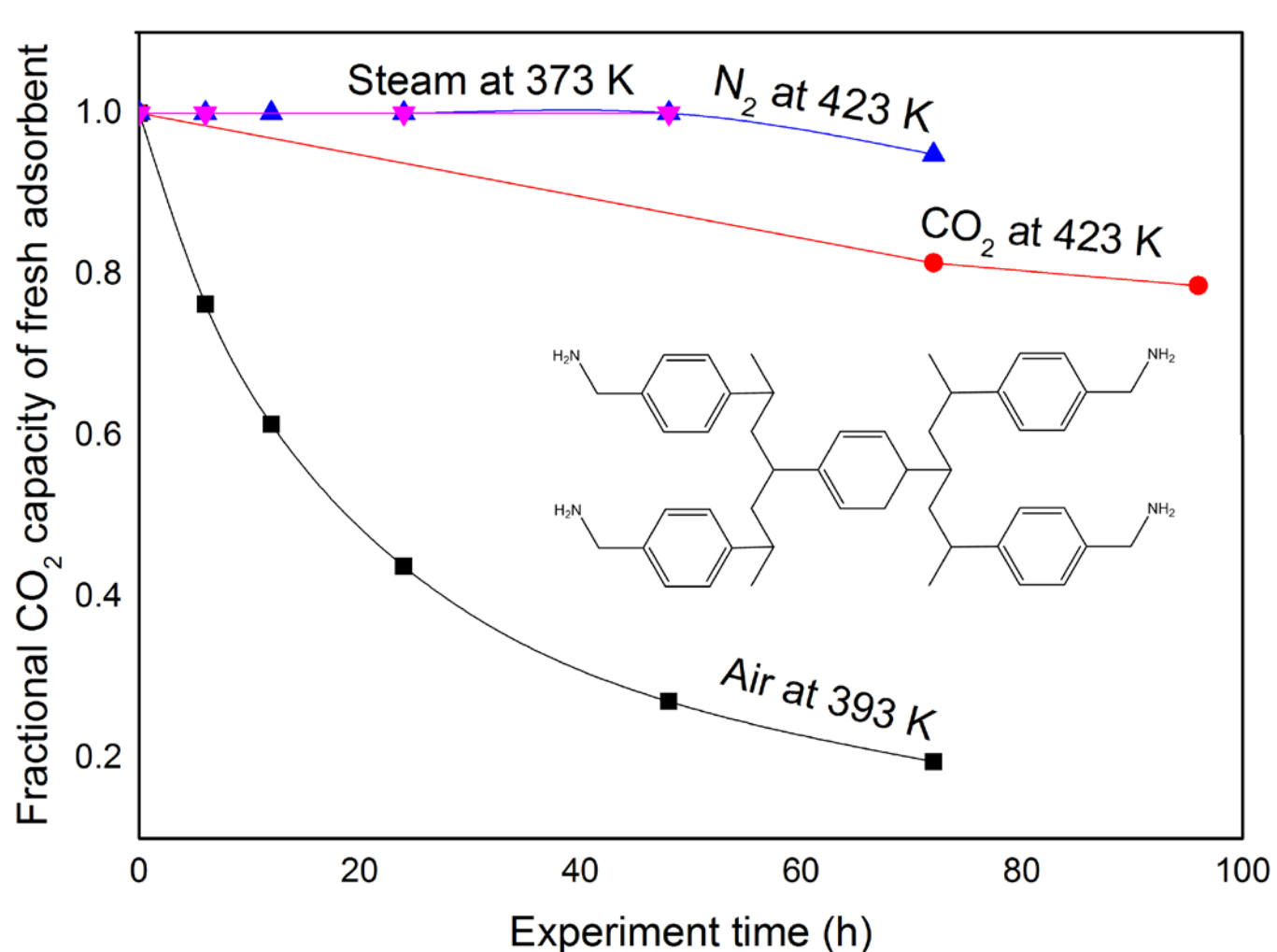


Figure 3: Sorbent stability in air, CO<sub>2</sub>, N<sub>2</sub> and H<sub>2</sub>O at elevated temperature.

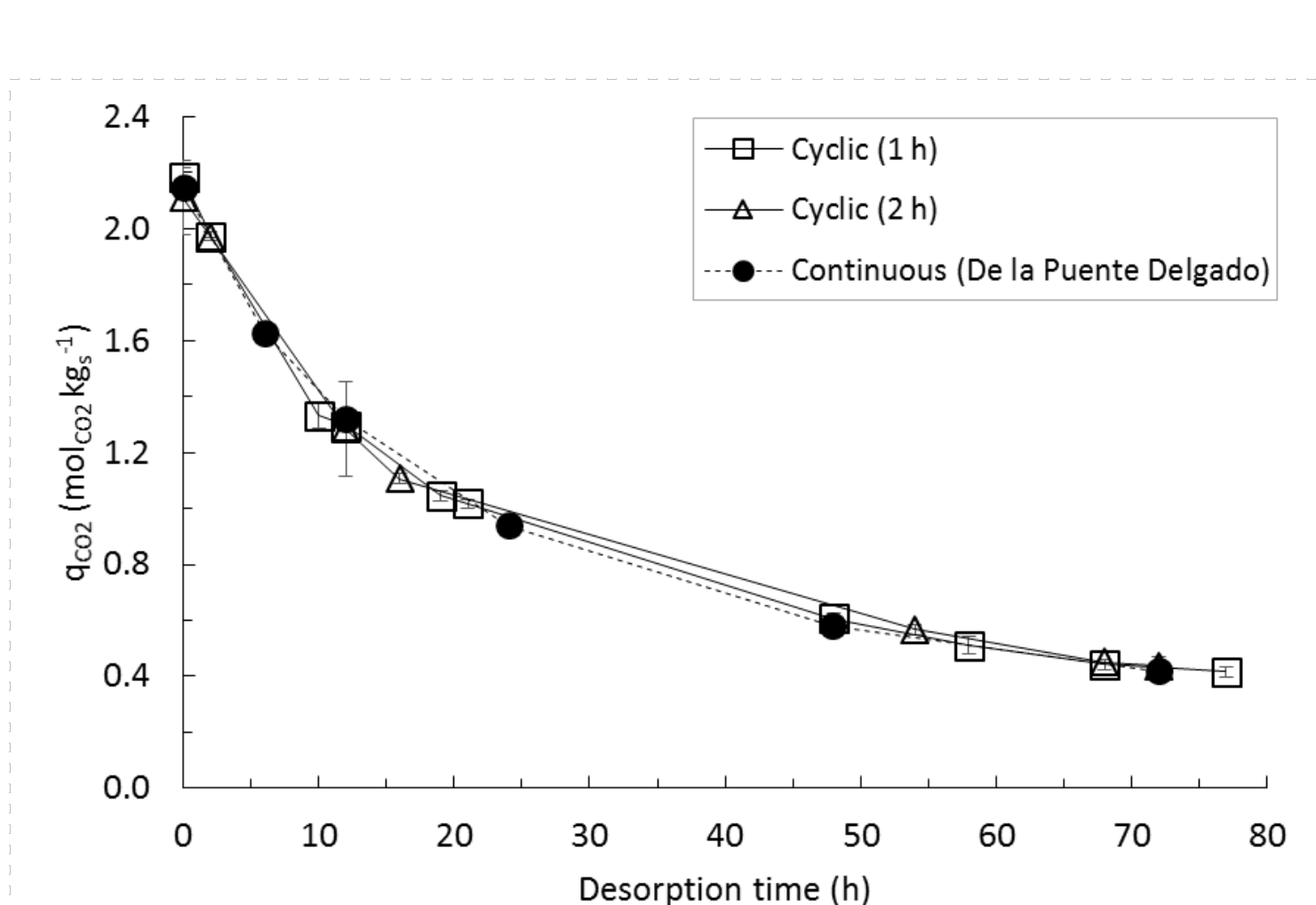


Figure 4: Comparison of cyclic treatment and continuous treatment in air at 120 °C.

## ... and much more work on...

sorbent CO<sub>2</sub> capacities, sorption kinetics, water co-adsorption, sorbent circulation and fluidization, optimization of regeneration conditions, process evaluation, ... resulting in :

## Pilot plant for CO<sub>2</sub> enriched air production

**Adsorber:** radial flow reactor

**Desorber:** moving fluid bed

**Desorption method:**

- ✓ Continuous sorbent in/out
- ✓ T regeneration: 60°C
- ✓ 1% CO<sub>2</sub> in product gas

## Evaluation

Air purge; 1 bar; T[K] = 333;

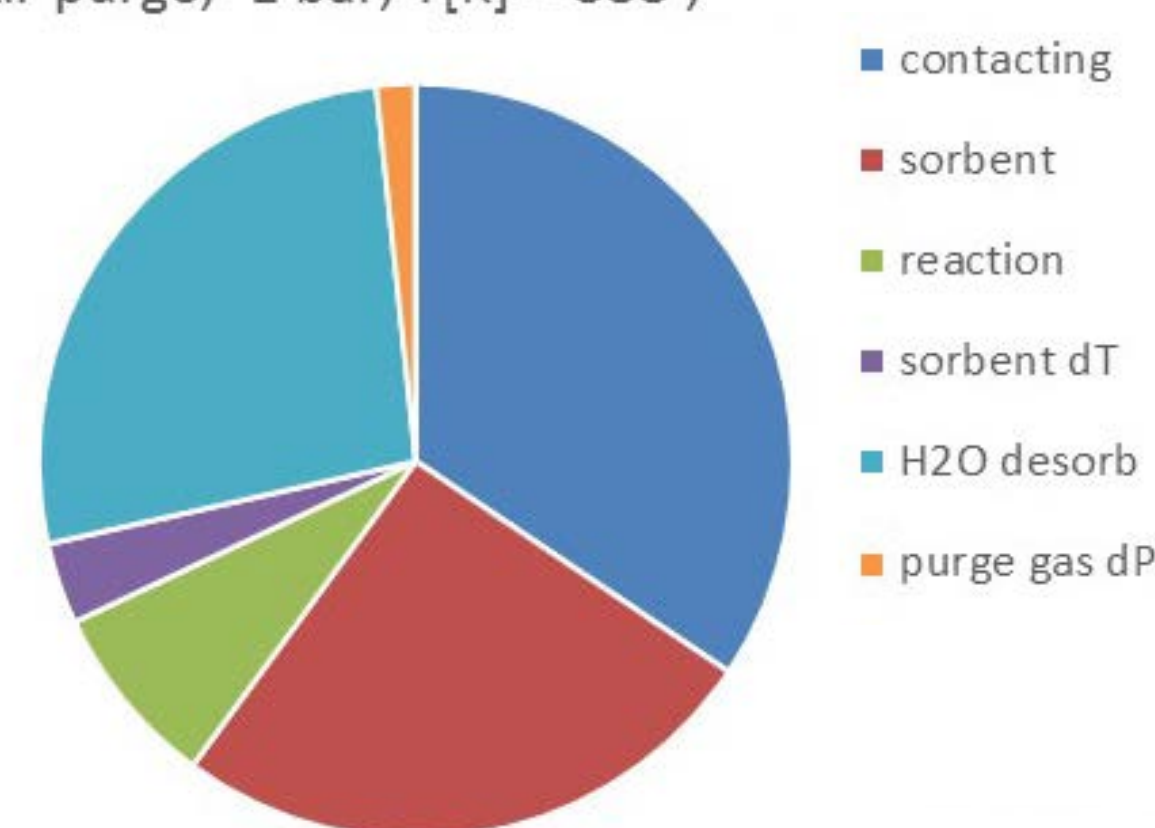


Figure 5: OpEx cost breakdown, based on energy needs and sorbent costs. No heat integration was included

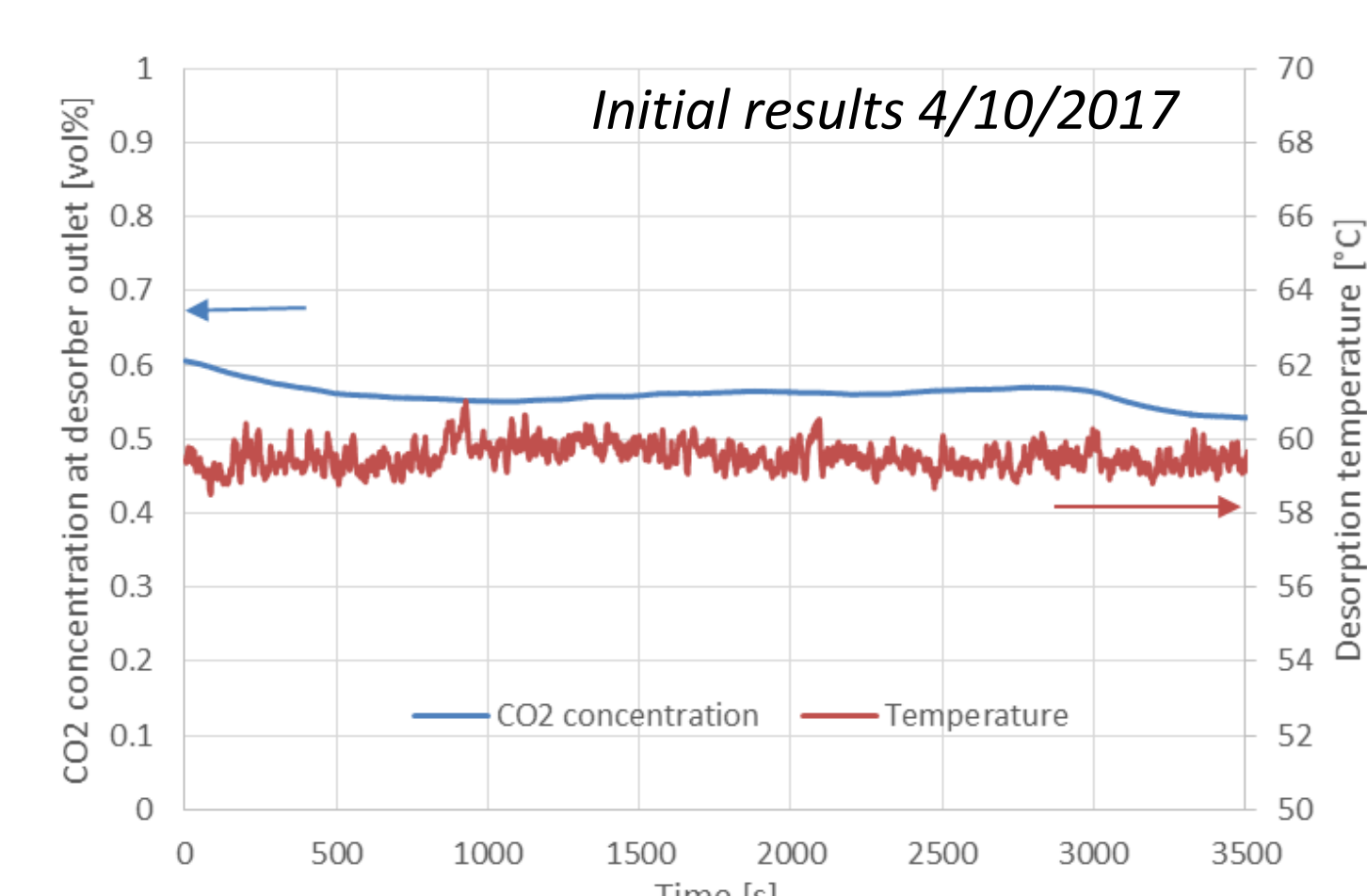


Figure 6: CO<sub>2</sub> concentration at the outlet of desorber and desorption temperature

## Acknowledgements



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